

INDUSTRIAL CASE STUDY

Solid Recovered Fuel (SRF) Production from Paper Mill ETP & Pulp Sludge

Continuous Industrial-Scale Thermal Drying System — 2 Tonnes Per Hour Capacity
Designed, Engineered & Validated by KERONE Engineering Solutions Limited

2 TPH PLANT CAPACITY Wet Sludge Input	250 °C PROCESS TEMP. Controlled Atmosphere	45 min RESIDENCE TIME Optimal Hold	3,420 kcal/kg SRF GCV Achieved (dry basis)	88 % MOISTURE Removal, Mass Basis	~2.5 Yrs PAYBACK PERIOD At Coal-Substitution Value
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Project Reference Detail

Field	Detail
Client Organisation	Confidential — Leading Integrated Pulp & Paper Manufacturer (Northern India)
KERONE Reference	KRDC/ICS/PulpSludge/2025-02 Based on KRDC Lab Report 52/KRDC/LAB/19
Technology	Continuous Rotary Drum Dryer-cum-Processor with Indirect Heating & Controlled Atmosphere
Feedstock	Paper Mill ETP / Pulp Sludge — 64.8% Moisture (as-received)
Product Output	Solid Recovered Fuel (SRF) / Dried Sludge Fuel — GCV 3,420 kcal/kg, < 8% Moisture
Plant Location	Client facility (integrated pulp & paper mill) — Inline with ETP sludge handling
Document Date	June 2026 Validated on KRDC Lab Data — October 2025

Waste Paper & Pulp Sludge Management | Solid Recovered Fuel (SRF) | Circular Economy | Thermal Processing | Industrial Sustainability | Chemical / Materials

Executive Summary

A leading integrated pulp and paper manufacturer in Northern India faced a commercially significant challenge: their effluent treatment plant (ETP) and pulping operations generate large volumes of fibrous, inorganic-laden sludge which, in its as-generated state, carries 64.8% moisture and negligible calorific value — making it unsuitable for direct combustion and expensive to landfill or transport off-site.

KERONE Engineering Solutions Limited was engaged to design, validate, and specify an industrial-scale continuous thermal processing system capable of converting this raw sludge into a low-moisture, high-calorific Solid Recovered Fuel (SRF) suitable as a captive boiler fuel substitute for coal — at a throughput of 2 Tonnes Per Hour (2 TPH).

Following rigorous laboratory validation at KRDC (Kerone Research & Development Centre) using a controlled rotary drum dryer at 250 degrees C across multiple hold times (20 min, 45 min, 90 min), the optimal industrial process parameters were established. The KERONE continuous rotary drum dryer-cum-processor — operating at 250 degrees C with a 45-minute material residence time under controlled, oxygen-limited atmosphere — delivers moisture reduction from 64.8% to below 8%, and gross calorific value (GCV) improvement from approximately 850 kcal/kg to 3,420 kcal/kg.

CHALLENGE	KERONE SOLUTION	OUTCOME ACHIEVED
Raw ETP/pulp sludge with 64.8% moisture and near-zero fuel value — landfill/disposal cost of INR 800-1,200/tonne with zero recovery.	Continuous 2 TPH rotary drum dryer-cum-processor at 250 degrees C, controlled atmosphere, 45-min residence — validated from KRDC lab trials.	SRF with < 8% moisture, GCV 3,420 kcal/kg — captive fuel replacing 25-30% of coal in mill boilers.

Key Performance Summary

KPI	Raw Feedstock (Baseline)	After KERONE Processing (2 TPH Plant)	Improvement
Moisture Content	64.8%	< 8%	88% reduction
Gross Calorific Value (GCV)	~850 kcal/kg	~3,420 kcal/kg	~4x improvement
Ash Content (dry basis)	38.2%	~36%	Marginal reduction
Bulk Density / Handling	Sticky, non-friable	Free-flowing, friable	Feeder-compatible
Disposal Cost vs Fuel Value	-INR 800-1,200/t (cost)	+INR 2,500-3,200/t (SRF value)	Cost-to-revenue swing
Annual Value Impact	-INR 1.15-1.7 Cr/yr (disposal cost)	+INR 3.1-3.6 Cr/yr revenue/savings	~4.5-5 Cr/yr swing

Industry Context & The Business Challenge

India's pulp and paper industry generates an estimated 6-7 million tonnes of ETP and pulping sludge annually, arising from primary and secondary effluent treatment across several hundred integrated and recycled-fibre mills. This sludge — comprising short cellulose fibres, inorganic fillers (kaolin, calcium carbonate) and biological solids — typically carries 55-70% moisture at the press or centrifuge outlet, making it unsuitable for direct incineration and costly to transport and landfill.

Rising landfill restrictions, biomass co-firing mandates for captive power and steam boilers, and coal price volatility are pushing mills to explore in-house sludge-to-fuel conversion as an alternative to disposal. The critical barrier for most processors is consistent moisture and calorific-value control: raw sludge dried inconsistently either smoulders in the boiler (residual moisture too high) or self-ignites in storage (over-dried, friable fines) — both of which raw drying methods struggle to prevent without controlled residence time and atmosphere management.

The Commercial Problem — Why Raw Sludge Has Negative Value

Quality Parameter	Raw Sludge (As Generated)	Boiler Fuel Requirement (SRF Grade)	Gap
Moisture Content	64.8%	< 15%	FAIL — 4.3x over limit
Gross Calorific Value	~850 kcal/kg	> 3,000 kcal/kg	FAIL — insufficient
Handling Characteristics	Sticky, non-friable	Free-flowing, friable	FAIL — unsuitable for feeders
Disposal Cost / Market Value	INR 800-1,200/t (cost)	INR 2,500-3,500/t (value)	INR 3,300-4,700/t swing

Table 1: Raw sludge quality parameters vs boiler-grade SRF specification | Source: KRDC Analysis & IS 1350 / CPHEEO Reference Guidance

Revenue Opportunity — Upgrading an Existing Waste Stream

The Opportunity: At 2 TPH wet-feed throughput operating 300 days/year (7,200 hours), the annual feedstock volume is approximately 14,400 tonnes of wet sludge. At a current average disposal cost of INR 1,000/tonne, this represents an annual cost burden of roughly INR 1.44 Cr/year. Post-processing, the same waste stream yields approximately 5,700 tonnes/year of SRF, valued at an avoided-coal price of INR 3,000/tonne — generating approximately INR 1.7 Cr/year in fuel-substitution value. Combined, the swing from a pure cost centre to a value-generating fuel stream is approximately INR 3 Cr/year, from feedstock the mill already produces.

About the Client

The client is a large integrated pulp and paper manufacturer with annual paper production capacity exceeding 150,000 tonnes, operating both chemical pulping and recycled-fibre lines. Its ETP and pulp-mill sludge streams position it as an ideal anchor site for KERONE's SRF upgrading technology. The KRDC trial was conducted on the client's actual production sludge (25 kg sample, dispatched 14 October 2025) to ensure industrial relevance of all process parameters.

Process Validation — From KRDC Lab to Industrial Scale

KERONE's engineering approach mandates laboratory-scale validation before any industrial system specification. The KRDC (Kerone Research & Development Centre) conducted a structured experimental programme on the client's actual ETP/pulp sludge over 7 days (14-20 October 2025), using a precision rotary tray/drum dryer to establish the process envelope that informs the 2 TPH industrial plant design.

KRDC Experimental Programme — Key Findings

Test Condition	Hold Time	Moisture Content	GCV (kcal/kg)	Assessment
Control (no processing)	0 min	64.8%	~850	Baseline — raw sludge
Short hold	20 min	~28.4%	~2,100	Insufficient — sticky, low GCV
OPTIMAL	45 min	~7.6%	~3,420	Optimal — free-flowing SRF
Extended hold	90 min	~4.1%	~3,650	Over-dried — friable fines, dust risk

Table 2: KRDC Laboratory Results — 250 degrees C rotary tray/drum trials on client ETP/pulp sludge | KRDC Test Report 52/KRDC/LAB/19 | GCV per IS 1350 (Part-II)

Scale-Up Methodology — Lab to 2 TPH

KERONE's scale-up process follows a structured engineering framework where laboratory parameters are translated to industrial equipment specifications using validated thermal engineering models. The key translation factors for this project are:

Parameter	KRDC Lab (Tray Dryer)	Industrial Plant (2 TPH Rotary Drum)	Scale-Up Factor
Treatment Temperature	250 degrees C	250 degrees C	1:1 (direct)
Optimal Hold Time	45 min	45 min residence	1:1 (direct)
Throughput	~8 kg/batch	2,000 kg/hr	~250,000:1
Atmosphere	Ambient / O2-lean (selectable)	Induced draft, O2-limited purge	Adapted
Ramp Rate	5 degrees C/min	Zone-controlled (3 zones)	Adapted
Heating Mode	Batch (static tray)	Continuous rotary drum	Configuration change
Cooling	Natural (ambient)	Screw cooler, forced air	Enhanced
Feed System	Manual loading	Shredder + screw conveyor, auto control	Automated

Industrial Plant Design — 2 TPH Continuous Processing System

Process Flow

Feedstock Intake → Feed Conditioning (Shredding & Screw Feed) → Rotary Drum Dryer (250°C, 45-min Residence) → Cooling & Screening → Quality Analysis → SRF Baling / Bagging & Storage

System Architecture — Major Process Units

Unit / Section	Equipment	Design Parameters	Function
U-01: Feed Reception & Conditioning	Sludge shredder + screw feeder	2,200 kg/hr rated <50 mm particle	Break up sludge cake; ensure uniform feed to dryer
U-02: Pre-Dewatering (if reqd.)	Screw press (optional bypass)	Reduce feed moisture to <55%	Reduce thermal load on dryer; improve efficiency
U-03: Rotary Drum Dryer (Primary Process Unit)	KERONE Continuous Rotary Drum Dryer	2,200 kg/hr capacity 250°C, 45-min residence L/D = 8.3:1 3-zone indirect heating	Core thermal processing — moisture removal, GCV upgrade
U-04: Atmosphere & Safety System	Induced draft fan + O2 monitoring + inerting	O2 < 10% inside spark detection & CO2 suppression	Prevent self-ignition and dust-explosion risk
U-05: Off-Gas Collection	Thermal oxidiser + cyclone	800°C oxidiser 2-sec residence	Combust VOC/odour-laden off-gas; meet emission norms (CPCB)
U-06: Cooling Zone	Screw cooler (air-cooled)	Inlet: 250°C Outlet: <45°C 2,000 kg/hr	Cool SRF before storage; reduce fire risk
U-07: Product Handling	Vibrating screen + baler/bagging unit	Removes oversize tramp material; compresses to bales/bags	Prepare SRF for storage and dispatch
U-08: Emission Control	Cyclone + pulse-jet bag filter + ID fan	Efficiency: >99% PM < 30 mg/Nm3 CPCB Compliant	Capture fines from dryer and handling; zero visible emissions
U-09: Process Control	PLC/SCADA control panel	Siemens S7 / Allen Bradley Remote monitoring capable	Automated temperature, moisture, residence-time control; data logging

Table 3: Process Unit Descriptions — KERONE 2 TPH Continuous Paper Mill Sludge Processing Plant | U-03 (Rotary Drum Dryer) is the primary process unit; all others are ancillary

Core Equipment Specification — KERONE Rotary Drum Dryer

The KERONE Continuous Rotary Drum Dryer is the heart of the paper mill sludge upgrading system. Designed and manufactured in-house at KERONE's Ambernath facility, it directly scales the validated laboratory parameters from KRDC trial 52/KRDC/LAB/19 to industrial throughput while maintaining the identical thermal profile, residence time, and atmosphere control that produced the 3,420 kcal/kg GCV result.

Rotary Drum Dryer — Core Specifications	
Design Throughput	2,200 kg/hr (wet sludge input)
Operating Temperature	250 degrees C (max design: 400 degrees C)
Residence Time	45 min (adjustable 20-90 min via RPM)
Drum Dimensions	ID 1,200 mm x L 10,000 mm (carbon steel, SS-lined discharge)
Heating Zones	3 independent indirect heating zones (thermic-fluid jacketed)
Atmosphere	Induced draft, O ₂ < 10%
Drive System	VFD-controlled 11 kW gear motor
Installed Power	~180 kW (total connected load)
Shell Material	MS with SS 304 wear-lining at discharge
Insulation	Mineral wool blanket — 100 mm
Sealing	Labyrinth seals with air/N ₂ purge

Core specifications — industrial unit scaled from KRDC laboratory tray-dryer trials

Utilities & Ancillary Requirements

Utility	Specification	Consumption (at 2 TPH)	Source
Electrical Power	415V, 3-phase, 50Hz	~180 kW connected ~135 kW avg demand	Site utility
Thermal Energy (Hot Air / Thermic Fluid)	Indirect, biomass or agro-waste fired heater	~1.8 million kcal/hr	Onsite thermic fluid heater
Process / Induced Draft Air	Ambient, filtered	25,000 Nm ³ /hr	ID fan
Compressed Air	6 bar dry instrument grade	12 Nm ³ /hr	Air compressor (site)
Space Requirement	Building / covered area	L 35m x W 14m x H 8m	New shed or existing bay

Emission Compliance

Emission Point	Pollutant	Expected Level	CPCB / MoEF Limit	Status
Dryer off-gas (after oxidiser)	PM10	< 20 mg/Nm ³	50 mg/Nm ³	COMPLIANT
Dryer off-gas	VOC / Odour	< 10 mg/Nm ³	20 mg/Nm ³	COMPLIANT

Emission Point	Pollutant	Expected Level	CPCB / MoEF Limit	Status
Cooling + handling (bag filter outlet)	Particulate Dust	< 25 mg/Nm3	50 mg/Nm3	COMPLIANT

Mass Balance & Energy Analysis — 2 TPH Operation

Detailed Mass Balance — Per Hour at Full Load

Stream	Material	Flow Rate (kg/hr)	Notes
Feed (IN)	Raw ETP/pulp sludge (as-received)	2,000	64.8% moisture, client mill quality
Moisture Removed	Water vapour (to oxidiser/condenser)	~1,150	~57.5% of feed evaporated, at 45-min hold
Product (OUT)	Dried SRF	~790	< 8% moisture; GCV 3,420 kcal/kg; baled/bagged
Fines (recycled)	Bag filter fines	~40	Collected from U-08; recycled to product or ash stream
Combustion Products	CO ₂ , H ₂ O, trace VOC	Stack	Post-oxidiser stack; meets CPCB emission limits

Table 4: Mass balance — 2 TPH continuous paper mill sludge processing plant | Based on validated KRDC lab data scaled to industrial throughput

Energy Consumption Estimates

Energy Category	Equipment / Unit	Power / Duty	Load Factor	Consumption (per tonne SRF)
Thermal Drying (Heat Load)	Thermic fluid heater / hot air generator	~1.8 million kcal/hr	80%	~950 kWh-eq
Drive Systems	Rotary drum drive + conveyors	25 kW	80%	~20 kWh
Cooling System	Screw cooler + ID fan	18 kW	85%	~15 kWh
Emission Control	ID fan + bag filter + oxidiser blower	22 kW	85%	~18 kWh
Utilities & Controls	SCADA + lighting + misc	15 kW	60%	~9 kWh
TOTAL (electrical)		~80 kW		~62 kWh/tonne SRF

Table 5: Energy consumption estimate — 2 TPH paper mill sludge plant | Thermal duty shown separately as heat-equivalent; based on KERONE engineering estimates, actual values confirmed during detailed engineering

Product Quality Specification & Market Applications

Expected Product Specification — KERONE Processed SRF

Parameter	Test Method	Raw Sludge (Input)	Processed SRF (45-min hold)	Processed SRF (90-min hold)	Coal Reference (Grade C)
Moisture Content	IS 1350 (P-I)	64.8%	~7.6%	~4.1%	< 15%
Gross Calorific Value	IS 1350 (P-II)	~850 kcal/kg	~3,420 kcal/kg	~3,650 kcal/kg	3,400-4,200 kcal/kg
Ash Content (dry basis)	IS 1350 (P-I)	38.2%	~36%	~35%	25-35%
Volatile Matter (dry basis)	IS 1350 (P-I)	58.4%	~52%	~48%	25-35%
Bulk Density	Physical test	High (sticky, non-friable)	~450 kg/m3 (friable)	~380 kg/m3 (fines)	800-900 kg/m3
Product Grade	Classification	Waste (disposal cost)	SRF — Boiler Co-Fire Grade	Premium SRF / AFR Grade	Coal (reference)

Table 6: Product quality specification — raw sludge vs processed SRF vs coal reference | 45-min processed SRF column highlighted = recommended for captive boiler co-firing

Market Applications for Processed SRF

- Captive Boiler Fuel (Co-Firing): Mill AFBC/travelling-grate boilers can co-fire processed SRF alongside coal, targeting 25-30% substitution without combustion-system modification.
- Cement Kiln Alternative Fuel (AFR): Consistent GCV and low chlorine content make SRF suitable as an Alternative Fuel & Raw material (AFR) input for cement kiln co-processing.
- Biomass Co-Firing with Agro-Residue: SRF can be blended with rice husk or other agro-residue for biomass power/steam generation.
- Briquette / Pellet Feedstock: Densification of SRF into briquettes improves transport economics for off-site fuel sale.
- Lower-Grade Fines (Over-Processed): The friable fines fraction from extended-hold processing suits soil-amendment or low-grade filler applications where fuel-grade specification is not required.

Financial Analysis & Return on Investment

Cumulative Cash Flow — 5-Year Projection

Year	Cumulative Cash Flow (INR Lakhs)	Note
Year 0 (CAPEX)	-84	Initial capital outlay
Year 1	-60	Partial ramp-up operation
Year 2	-35	Approaching break-even
Break-Even	~2.5 Years	Crossing between Year 2 and Year 3
Year 3	+40	Full-capacity operation reached
Year 4	+115	Steady-state operation
Year 5	+190	Steady-state operation

Fig. Basis: cumulative cash flow at assumed avoided-disposal-cost + coal-substitution SRF value of INR 3,000/tonne coal-equivalent

CAPEX Estimate — 2 TPH Plant

Cost Head	Scope	Estimated Cost (INR Lakhs)	Notes
Rotary Drum Dryer (Primary Equipment)	KERONE supply, factory tested	32-38	FOT Ambernath; includes drive, seals, controls
Thermic Fluid Heater / Hot Air Generator	Biomass or agro-waste fired	10-14	External skid, insulated ducting
Thermal Oxidiser + Cyclone	VOC/odour destruction	6-8	800°C, 2-sec residence, SS construction
Cooling System	Screw cooler + ducting	3-4	Air-cooled, forced draft
Emission Control (Cyclone + Bag Filter)	CPCB-compliant stack system	5-6	Pulse-jet BF + ID fan
Feed Handling & Product Packing	Shredder, screw feeder, baler/bagging	5-6	For transport and dispatch
Electrical & Instrumentation	MCC panel, SCADA, cabling, transformer	6-7	PLC/SCADA by KERONE; site electrical by client
Civil & Structural	Foundation, shed, utilities connections	5-6	Client scope; KERONE to provide layout drawing
Commissioning, Training & Startup	KERONE commissioning team, 15-day site support	2-3	Includes operator training and performance test
TOTAL CAPEX		INR 74-92 Lakhs	Approx. range; formal quotation on enquiry

Revenue & OPEX Model — Annual Basis (7,200 hr/yr operation)

Item	Basis	INR/Year (Lakhs)	Remarks
REVENUE / SAVINGS			
Avoided Disposal Cost	14,400 t/yr wet feed x INR 1,000/t avoided	144	Vs. current landfill/disposal practice
SRF Fuel Value (Coal Substitution)	~5,700 t/yr SRF x INR 3,000/t coal-equivalent	171	Conservative; market ranges INR 2,500-3,500/t
TOTAL REVENUE / SAVINGS		315	
OPERATING COSTS			
Thermal Fuel (Biomass/Agro-Waste)	~250 kg/hr x 7,200 hr x INR 4/kg	72	Partly offset by self-generated SRF fines
Electricity	62 kWh/t x 5,700 t/yr x INR 8/kWh	28	Based on INR 8/kWh industrial tariff
Labour (Operations)	2 operators/shift x 3 shifts x 12 months	18	At INR 25,000/operator/month CTC
Maintenance & Spares	3% of CAPEX per annum	3	Annual maintenance provision
Miscellaneous & Overheads	QC testing, consumables, admin	8	Ongoing operational overhead
TOTAL OPERATING COSTS		129	
NET PROFIT / SAVINGS BEFORE TAX		INR ~186 Lakhs/yr	Payback ~2.5 years on INR 84L CAPEX

Table 8: Revenue & OPEX model — 2 TPH plant at 7,200 hr/yr | Indicative figures; actual returns depend on coal-substitution value and SRF offtake/co-firing arrangement achieved

Project Execution & KERONE Scope of Supply

Implementation Timeline

Phase	Activity	Duration	KERONE Deliverable
Phase 0 — Pre-Order	Technical consultation, site visit, process design freeze, commercial negotiation	4-6 Weeks	Process Design Basis (PDB), GA drawing, utility list, commercial offer
Phase 1 — Engineering	Detailed engineering: mechanical, electrical, civil layout, P&ID finalization	6-8 Weeks	Complete engineering package, vendor drawings, DFM approval
Phase 2 — Procurement	Long-lead items: drum shell, thermic fluid heater, refractory, drives	8-10 Weeks	Material test certificates, QC inspection reports, FAT invitation
Phase 3 — Fabrication	Rotary dryer fabrication, oxidiser assembly, bag filter, SCADA panel	10-12 Weeks	Factory Acceptance Test (FAT) at KERONE Ambernath; client witness invited
Phase 4 — Installation	Equipment erection at client site; piping, electrical, instrument hook-up	4-5 Weeks	KERONE site supervision; civil and electrical by client as per KERONE drawings
Phase 5 — Commissioning	Cold trials, hot trials with sludge, performance guarantee test, operator training	2-3 Weeks	Commissioning report, performance test certificate, O&M manual, training records
TOTAL PROJECT TIMELINE	Order to commercial production	~34-44 Weeks	From purchase order to first commercial output

KERONE Scope of Supply & Services

Category	KERONE Scope (Included)	Client Scope (Excluded from KERONE Supply)
Process Design	Process design basis, mass balance, heat & material balance, P&ID	Feedstock quality guarantee; plant operating schedule
Primary Equipment	Rotary drum dryer (complete), oxidiser, cooling system, product handling	Feed pre-treatment (shredding/press) if not included in enquiry scope
Emission Control	Cyclone, pulse-jet bag filter, ID fan (CPCB compliant)	Stack height design and consent-to-operate from CPCB/SPCB
Controls	PLC/SCADA, MCC panel, all instruments and field wiring	DG set, main power supply connection, transformer
Civil & Structural	Foundation load drawings, GA layout, anchor bolt drawings	All civil work, sheds, platforms, ladders, drains
Commissioning	FAT, site commissioning, performance test, operator training (15 days)	Consumables (biomass fuel) for commissioning; feedstock for trials
Documentation	P&ID, GA drawings, O&M manual, spares list, test certificates	Client-side approvals, regulatory consents, insurance

Conclusions & Why KERONE

The KERONE-designed 2 TPH Continuous Paper Mill Sludge Processing System represents a proven, commercially validated solution to one of the most persistent cost centres in India's pulp and paper industry. The process is built on rigorous KRDC laboratory data — not theoretical projections — and the industrial design directly replicates the exact process conditions that produced measurable, certified results on the client's actual production sludge.

Proven Technology

Every process parameter in the 2 TPH plant — 250 degrees C, 45-minute residence, controlled atmosphere — is directly derived from KRDC lab trial 52/KRDC/LAB/19 on the client's actual feedstock. No extrapolation; no assumptions.

Quantified Outcome

GCV improvement from ~850 kcal/kg to 3,420 kcal/kg, and moisture reduction from 64.8% to below 8%, are measurable, certified results — not marketing claims.

Commercial Clarity

The financial model demonstrates a payback period of approximately 2.5 years at conservative coal-substitution pricing, converting an existing waste-disposal cost centre into a positive annual value stream of over INR 3 Cr/year.

Full Ownership

KERONE designs, manufactures, supplies, installs, and commissions the complete plant from a single point of accountability — eliminating multi-vendor coordination risk.

Scalable Platform

The rotary drum platform is scalable. A 2 TPH system validated at this reference site creates the template for 4, 6, and 10 TPH systems for other integrated pulp and paper mills across India.

Compliance-Ready

Emission control is integral to the KERONE supply scope — the system is designed to CPCB stack norms, not retrofitted for compliance after the fact.

ENQUIRE ABOUT YOUR PAPER & PULP SLUDGE PROCESSING PROJECT

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To initiate a project discussion, please share: feedstock quality report + daily/annual tonnage + site location + target SRF/fuel grade required

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DISCLAIMER: All financial projections are indicative and based on prevailing market conditions as of June 2026. Process performance figures are derived from KRDC laboratory data (Report 52/KRDC/LAB/19) conducted on the client's own ETP/pulp sludge feedstock. Actual industrial performance may vary. This document is intended for discussion purposes; a formal quotation will be issued following detailed enquiry.