

INDUSTRIAL CASE STUDY

Continuous Paper Web Drying & Heat Recovery Systems

Continuous Industrial-Scale Dryer Section Upgrade — 200 Tonnes Per Day (TPD) Kraft Paper Machine
Designed, Engineered & Validated by KERONE Engineering Solutions Limited

200 TPD PLANT CAPACITY Finished Kraft Paper	65 % RECOVERY HOOD EXHAUST Heat Recovered	1.45 kg/kg SPECIFIC STEAM Consumption Achieved	24.5 % SPECIFIC ENERGY Reduction vs Baseline	~2.3 Yrs PAYBACK PERIOD On Fuel Savings
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PROJECT REFERENCE DETAIL	
Client Organisation	Shree Ganesh Paper & Boards Ltd. — Kraft/Packaging Paper Manufacturer
KERONE Reference	KRDC/ICS/PaperDry/2025-02 Based on KRDC Trial Report 52/KRDC/LAB/22
Technology	Multi-Cylinder Dryer Section Optimisation with Closed Hood & Air-to-Air Heat Recovery
Feedstock / Input	Pressed Paper Web — 62% Moisture Content (post-press, as-received)
Product Output	Kraft Packaging Paper — 6.0% ± 0.3% Final Moisture Content
Plant Location	Client facility (integrated paper mill) — Retrofit on existing Paper Machine (PM-1)
Document Date	July 2026 Validated on KRDC Pilot Trial Data — November 2025

Pulp & Paper | Dryer Section Retrofit | Waste Heat Recovery | Energy Efficiency | Industrial Sustainability | Chemical / Process Industries

Executive Summary

Shree Ganesh Paper & Boards Ltd., an established Indian kraft and packaging paper manufacturer, operates a 200 TPD paper machine (PM-1) whose dryer section — the single most energy-intensive stage of the papermaking process — was consuming steam well above industry benchmarks. The existing multi-cylinder dryer operated with a uniform steam pressure profile and an open hood that vented exhaust air directly to atmosphere at 130-140 degrees C, discarding a large fraction of usable process heat and resulting in a specific steam consumption of 1.92 kg steam per kg of paper produced, against an achievable benchmark of below 1.5 kg/kg for modern high-efficiency dryer sections.

KERONE Engineering Solutions Limited was engaged to design, validate, and specify a continuous dryer-section upgrade combining optimised multi-zone steam pressure profiling, a closed hood system, and an air-to-air heat recovery exchanger (runaround coil) to recover hood exhaust heat for preheating fresh make-up air and boiler combustion air — without altering the existing paper machine's mechanical envelope.

Following a structured on-site pilot validation programme at KRDC (Kerone Research & Development Centre) using an instrumented test rig on the client's actual PM-1 dryer section across multiple configurations, the optimal industrial process parameters were established. The KERONE-designed system — a 4-zone graduated steam pressure profile (2.5 to 4.5 bar) combined with 65% hood exhaust heat recovery — reduces specific steam consumption from 1.92 kg/kg to 1.45 kg/kg, and improves exit moisture uniformity from $\pm 1.2\%$ to $\pm 0.3\%$.

CHALLENGE	KERONE SOLUTION	OUTCOME ACHIEVED
Dryer section running at 1.92 kg steam/kg paper with hood exhaust vented to atmosphere at 130-140 degrees C — no heat recovery, inconsistent exit moisture ($\pm 1.2\%$).	4-zone graduated steam pressure profiling with closed hood and air-to-air heat recovery exchanger — validated from KRDC on-site pilot trials.	1.45 kg steam/kg paper, 65% hood heat recovered, $\pm 0.3\%$ moisture uniformity — INR ~2.4 Cr/yr fuel cost saving.

Key Performance Summary

KPI	Baseline (Before)	After KERONE Processing (200 TPD Plant)	Improvement
Specific Steam Consumption	1.92 kg/kg paper	1.45 kg/kg paper	24.5% reduction
Exit Web Moisture Content	7.8% $\pm$ 1.2%	6.0% $\pm$ 0.3%	Uniformity improved 4x
Hood Exhaust Heat Recovered	0% (fully vented)	65% recovered	New capability
Specific Thermal Energy	1,050 kcal/kg paper	792 kcal/kg paper	24.5% reduction
Sustainable Machine Speed	480 m/min	520 m/min	+8.3% throughput
Annual Fuel Cost (Coal-fired boiler)	INR 9.8 Cr/yr	INR 7.4 Cr/yr	INR 2.4 Cr/yr saving

Industry Context & The Business Challenge

India's paper industry represents an installed capacity of approximately 25 million tonnes per annum, with packaging and kraft paper the largest and fastest-growing segment, expanding at 6-7% CAGR on the back of e-commerce and FMCG packaging demand. The drying section of a paper machine is universally recognised as the most energy-intensive stage of production, typically accounting for 65-75% of total process steam consumption across the mill.

In conventional multi-cylinder dryer sections, hood exhaust air — laden with moisture evaporated from the paper web — is commonly vented directly to atmosphere at 120-140 degrees C, discarding 25-40% of the total heat input to the dryer section as unrecovered waste heat. With coal and biomass fuel costs having risen steadily and ESG-linked packaging mandates from FMCG brand owners increasingly scrutinising the carbon footprint of paper suppliers, the specific energy consumption of the dryer section has become a direct commercial and competitive liability for mills that have not modernised.

The Commercial Problem — Why the Existing Dryer Section Under-performs

Quality Parameter	Existing Dryer Section (Shree Ganesh)	Benchmark (Modern High-Efficiency Dryer)	Gap
Specific Steam Consumption	1.92 kg steam/kg paper	< 1.50 kg steam/kg paper	FAIL — 28% over benchmark
Hood Exhaust Heat Recovery	0% (vented to atmosphere)	50-70% typical recovery	FAIL — no recovery installed
Exit Moisture Variation	± 1.2%	± 0.3% or better	FAIL — quality & runnability risk
Specific Thermal Energy	1,050 kcal/kg paper	< 820 kcal/kg paper	FAIL — 28% excess energy use

Table 1: Existing dryer section performance vs modern benchmark | Source: KRDC On-Site Energy Audit & CPPRI Guidelines

Savings Opportunity — Retrofitting an Existing Asset

The Opportunity: At 200 TPD throughput operating 300 days/year (60,000 tonnes/year of finished paper), the existing dryer section consumes approximately 1.92 kg steam per kg of paper, equivalent to 115,200 tonnes of steam annually. KERONE's retrofit reduces this to 1.45 kg/kg, or 87,000 tonnes of steam annually — a reduction of 28,200 tonnes of steam per year. At the client's coal-fired boiler fuel cost basis, this converts to a fuel cost saving of approximately INR 2.4 Cr per year, without any change to finished paper grade, machine width, or production capacity.

About Shree Ganesh Paper & Boards Ltd.

Shree Ganesh Paper & Boards Ltd. is an established Indian manufacturer of kraft and packaging-grade paper, operating a single paper machine (PM-1) with a 4.2 m deckle width and rated capacity of 200 TPD. The mill's operations span pulping, stock preparation, wet-end forming, pressing, and drying, with the dryer section retrofit positioned as the highest-return energy efficiency intervention identified across the mill. The KRDC on-site trial was conducted using PM-1's actual operating conditions and instrumented hood exhaust monitoring to ensure industrial relevance of all process parameters.

Process Validation — From KRDC Pilot Trial to Industrial Scale

KERONE's engineering approach mandates on-site validation before any industrial system specification. The KRDC (Kerone Research & Development Centre) team conducted a structured on-site pilot programme on Shree Ganesh Paper & Boards' actual PM-1 dryer section over 6 days (10-15 November 2025), using an instrumented test configuration across the existing cylinder groups to establish the process envelope that informs the full-scale retrofit design.

KRDC On-Site Trial Programme — Key Findings

Test Condition	Hood Exhaust Temp. (Post-System)	Steam Pressure Profile	Specific Steam Consumption	Assessment
Baseline (existing)	138°C (fully vented)	Uniform 3.5 bar, all groups	1.92 kg/kg	Baseline — no recovery
Trial 1 — pressure profiling only	132°C (fully vented)	Graduated 2.5 → 4.5 bar	1.71 kg/kg	Improved; no heat recovery
Trial 2 — partial heat recovery	95°C (40% recovered)	Graduated 2.5 → 4.5 bar	1.58 kg/kg	Good; recovery limited by exchanger size
OPTIMAL — full-scale configuration	68°C (65% recovered)	Graduated 2.5 → 4.5 bar, 4 zones	1.45 kg/kg	Recommended for industrial design

Table 2: KRDC On-Site Trial Results — PM-1 dryer section, Shree Ganesh Paper & Boards | KRDC Trial Report 52/KRDC/LAB/22

Scale-Up Methodology — Pilot to Full 200 TPD Machine

KERONE's scale-up process follows a structured engineering framework in which pilot-validated parameters are translated to full-machine equipment specifications using validated drying and heat-transfer models. The key translation factors for this project are:

Parameter	KRDC Pilot Trial	Industrial Plant (200 TPD PM-1)	Scale-Up Factor
Dryer Cylinders Instrumented	8 (test section only)	42 (full dryer section)	Direct extrapolation
Web Width	0.6 m (slit test strip)	4.2 m (full deckle)	7:1
Heat Recovery Exchanger	Skid-mounted air-to-air unit	Full runaround-coil system, 48,000 Nm ³ /hr	Scaled to full hood airflow
Steam Pressure Zones	2 (manually controlled)	4 (PLC-automated, graduated 2.5-4.5 bar)	Configuration upgrade
Condensate / Flash Recovery	Not instrumented at pilot	Integrated flash vessel + LP steam header	New addition at full scale

Industrial Plant Design — 200 TPD Dryer Section Retrofit

The KERONE retrofit is engineered to fit within the existing paper machine's mechanical footprint, requiring no relocation of the press section, reel, or building structure. The system architecture comprises the following major process units, integrated with the mill's existing steam and condensate network:

System Architecture — Major Process Units

Unit / Section	Equipment	Design Parameters	Function
U-01: Press Section Interface	Existing press rolls (unmodified)	62% moisture web entry 4.2 m width	Delivers pressed web to dryer section at consistent solids content
U-02: Dryer Group 1 (Pre-Dryers)	12 steam-heated cylinders	2.5-3.0 bar 1.83 m dia.	Initial moisture removal; gentle ramp to avoid web cockle
U-03: Dryer Groups 2-4 (Main & After-Dryers)	30 steam-heated cylinders	3.5-4.5 bar graduated 1.83 m dia.	Bulk moisture removal to target 6.0% exit moisture
U-04: Closed Hood System	Insulated pocket-ventilated hood	Design temp. 140°C Class 1 hood seal	Contains evaporated moisture; enables controlled exhaust extraction
U-05: Heat Recovery Exchanger	Air-to-air runaround coil (glycol loop)	48,000 Nm ³ /hr 65% recovery efficiency	Recovers hood exhaust heat to preheat make-up/combustion air
U-06: Condensate & Flash Steam Recovery	Flash vessel + LP steam header	4.5 bar HP condensate flashed to 1.2 bar LP	Recovers flash steam for low-pressure mill users
U-07: Make-Up Air / Combustion Air Preheat	Ducted preheat coil to boiler FD fan	Ambient 32°C preheated to 58°C	Reduces boiler fuel demand using recovered heat
U-08: Moisture Profiling & Scanner System	Traversing infrared moisture scanner	CD profile ± 0.3% target	Closed-loop steam-zone trimming for uniform exit moisture
U-09: Process Control	PLC/SCADA integration with existing DCS	Siemens S7 / remote monitoring capable	Automated steam-zone, hood, and heat-recovery control; data logging

Table 3: Process Unit Descriptions — KERONE 200 TPD Dryer Section Retrofit | U-02/U-03 (dryer cylinders) and U-05 (heat recovery exchanger) are the primary process units

Core Equipment Specification — Heat Recovery Exchanger & Dryer Controls

The air-to-air runaround-coil heat recovery exchanger is the centrepiece of the retrofit. Designed and specified by KERONE to interface with the existing hood ductwork without structural modification, it directly scales the validated pilot parameters from KRDC trial 52/KRDC/LAB/22 to the full 48,000 Nm³/hr hood exhaust airflow while maintaining the identical recovery efficiency and pressure-profile logic that produced the 1.45 kg/kg steam consumption result.

Heat Recovery Exchanger — Core Specifications

Parameter	Specification
Design Airflow (Hood Exhaust Side)	48,000 Nm ³ /hr
Exhaust Inlet / Outlet Temperature	138°C in / 68°C out (65% recovery)
Make-Up Air Preheat	32°C ambient → 58°C preheated
Heat Transfer Medium	Glycol runaround loop (closed circuit)
Coil Construction	Finned-tube, SS 304 tube / aluminium fin
Pressure Drop (Airside)	< 250 Pa per coil bank
Circulation Pump	2 x 100% duty/standby, 15 kW each
Fouling Allowance	Self-cleaning fin spacing for fibrous dust loading
Control	Modulating 3-way valve, PLC-linked to exhaust temperature setpoint

Utilities & Ancillary Requirements

Utility	Specification	Consumption (at 200 TPD)	Source
Process Steam	4.5 bar saturated, graduated 2.5-4.5 bar across zones	12,079 kg/hr at optimised rate	Existing mill boiler house
Electrical Power	415V, 3-phase, 50Hz	~45 kW connected (fans, pumps, controls)	Site utility
Condensate Return	HP condensate to flash vessel	~11,500 kg/hr	Recovered to boiler feed / LP header
Compressed Air	6 bar dry, instrument grade	8 Nm ³ /hr	Air compressor (site)
Cooling / Glycol Loop	Closed-loop, no fresh water make-up	6 m ³ loop volume	Self-contained skid
Space Requirement	Roof-level ductwork + ground-floor skid	L 8m x W 4m x H 3m (exchanger skid)	Existing hood roof / adjacent bay

Emission & Environmental Compliance

Parameter	Expected Result	Requirement / Reference	Status
Boiler Fuel Consumption (coal-equivalent)	24.5% reduction	Mill energy-efficiency target	ACHIEVED
Specific CO ₂ Emissions (per tonne paper)	~24% reduction	Corporate ESG / brand-owner packaging mandates	ACHIEVED
Hood Fugitive Emissions	No increase; closed hood improves containment	Factory environmental clearance	COMPLIANT

Mass Balance & Energy Analysis — 200 TPD Operation

Detailed Mass Balance — Per Hour at Full Load

Stream	Material	Flow Rate (kg/hr)	Notes
Feed (IN)	Pressed paper web (as-received)	20,617	62% moisture, post-press solids ~38%
Water Evaporated	Moisture removed in dryer section	12,280	Reduced from 62% to 6.0% exit moisture
Product (OUT)	Finished kraft paper	8,330	6.0% ± 0.3% moisture; reeled
Broke / Trim (recycled)	Edge trim & web breaks to pulper	~7	Recycled to stock preparation; not a loss
Steam Consumed	Process steam to dryer cylinders	12,079	1.45 kg steam/kg paper at optimised rate
Condensate Returned	HP condensate to flash vessel	~11,500	~95% of steam condensed and returned

Table 4: Mass balance — 200 TPD continuous paper machine dryer section | Based on validated KRDC pilot data scaled to industrial throughput

Thermal Energy Distribution

Energy Category	Equipment / Stream	Share of Dryer Section Heat Demand	Specific Energy (kcal/kg paper)
Dryer Group 1 (Pre-Dryers)	12 steam cylinders, 2.5-3.0 bar	22%	174
Dryer Groups 2-4 (Main/After)	30 steam cylinders, 3.5-4.5 bar	58%	459
Hood Ventilation & Fan Load	Exhaust/supply fans, ducting	8%	63
Heat Recovery Credit	Air-to-air exchanger (recovered, netted out)	-24.5% (net saving)	-258
Net Specific Thermal Energy	—	—	792

Table 5: Thermal energy distribution — 200 TPD paper machine dryer section | Based on KERONE engineering estimates from KRDC trial data

Savings Summary — Steam & Fuel

Parameter	Baseline	After KERONE System	Annual Impact (60,000 t/yr paper)
Specific Steam Consumption	1.92 kg/kg	1.45 kg/kg	28,200 t/yr steam saved
Specific Thermal Energy	1,050 kcal/kg	792 kcal/kg	15.5 x 10 ⁹ kcal/yr saved
Coal-Equivalent Fuel (approx.)	—	—	~3,100 tonnes coal/yr saved
Fuel Cost Saving (at site tariff)	—	—	INR ~2.4 Cr/yr

Process Outcome Specification & Applications of Recovered Heat

Expected Process Outcome — KERONE-Upgraded Dryer Section

Parameter	Existing (Baseline)	After Pressure Profiling Only	After Full KERONE System	Industry Benchmark
Exit Moisture Content	7.8% ± 1.2%	7.2% ± 0.7%	6.0% ± 0.3%	6.0% ± 0.3% or better
Specific Steam Consumption	1.92 kg/kg	1.71 kg/kg	1.45 kg/kg	< 1.50 kg/kg
Sustainable Machine Speed	480 m/min	495 m/min	520 m/min	> 500 m/min
Web Breaks (per day, avg.)	3.2	2.1	1.0	< 1.5
Hood Exhaust Heat Recovered	0%	0%	65%	50-70%

Table 6: Process outcome comparison — baseline vs interim vs fully-optimised KERONE system | Reduced web breaks reflect improved moisture uniformity and web strength

Applications of the Recovered Heat

- **Boiler Combustion Air Preheat** — Recovered hood exhaust heat preheats the boiler's forced-draft combustion air from ambient (32°C) to 58°C, directly reducing coal or biomass fuel demand for the same steam output.
- **Fresh Make-Up Air Preheat** — Preheated make-up air supplied back into the dryer hood reduces the steam load otherwise needed to bring incoming ambient air up to process temperature.
- **Process / Wash Water Preheating** — A secondary low-grade heat tap can preheat stock-preparation wash water, reducing steam demand elsewhere in the mill.
- **Mill Building Space Heating** — In cooler climates or winter operation, a portion of recovered heat can be diverted to space-heating of adjacent process buildings.
- **Effluent Treatment Plant (ETP) Heating** — Low-grade recovered heat can support biological treatment stages in the ETP that benefit from moderate temperature elevation.

Financial Analysis & Return on Investment

CAPEX Estimate — 200 TPD Dryer Section Retrofit

Cost Head	Scope	Estimated Cost (INR Lakhs)	Notes
Heat Recovery Exchanger (Primary Equipment)	KERONE supply, factory tested	22-26	Runaround coil, glycol skid, pumps, controls
Hood Modification & Sealing	Closed hood upgrade, ducting	8-10	Class 1 seal, insulated ductwork
Condensate & Flash Steam System	Flash vessel, LP header tie-in	5-6	SS construction, safety valves
Steam Zone Automation	Control valves, 4-zone PLC integration	6-8	Integration with existing DCS
Moisture Scanner & Profiling System	Traversing IR scanner, CD control	9-11	Closed-loop trim control
Electrical & Instrumentation	MCC panel, cabling, field instruments	4-5	PLC/SCADA by KERONE; site electrical by client
Civil & Structural	Skid foundation, ductwork supports	3-4	Client scope; KERONE to provide layout drawing
Commissioning, Training & Startup	KERONE commissioning team, 10-day site support	3-4	Includes operator training and performance test
TOTAL CAPEX		60-74	Approx. range; detailed quote on enquiry

Table 7: CAPEX estimate — 200 TPD dryer section retrofit | All figures indicative; formal quotation on receipt of detailed enquiry

Revenue & OPEX Impact Model — Annual Basis (7,200 hr/yr operation)

Item	Basis	INR/Year (Lakhs)	Remarks
Fuel Cost Savings (Coal-fired boiler)	28,200 t/yr steam saved at delivered fuel cost	240	Primary saving driver
Reduced Web Breaks / Downtime Recovery	2.2 fewer breaks/day x uptime value	35	Improved runnability from uniform moisture
Electrical Power (Additional)	Fans, pumps, controls — added load	(9)	Incremental consumption of new equipment
Maintenance & Spares	3% of CAPEX per annum	(2)	Annual maintenance provision
NET ANNUAL BENEFIT		~264	Payback ~2.3 years on INR 67L CAPEX (mid-range)

Table 8: Revenue & OPEX impact model — 200 TPD plant at 7,200 hr/yr | Indicative figures; actual savings depend on fuel price and operating hours

Cumulative Cash Flow — 5-Year Projection

Year	Annual Net Benefit (INR Lakhs)	Cumulative Cash Flow (INR Lakhs)	Notes
Year 0 (CAPEX)	—	(67)	Mid-range CAPEX outlay
Year 1	264	197	First full year of operation
Year 2	264	461	Break-even achieved within Year 1
Year 3	264	725	
Year 4	264	989	
Year 5	264	1,253	

Table 9: Cumulative cash flow — 200 TPD dryer section retrofit, 5-year projection | Break-even within Year 1, ~2.3 years including ramp-up conservatism

Project Execution & KERONE Scope of Supply

Implementation Timeline

Phase	Activity	Duration	KERONE Deliverable
Phase 0 — Pre-Order	Technical consultation, site energy audit, process design freeze, commercial negotiation	3-4 Weeks	Process Design Basis (PDB), GA drawing, utility list, commercial offer
Phase 1 — Engineering	Detailed engineering: exchanger design, ducting layout, control philosophy, P&ID finalisation	5-6 Weeks	Complete engineering package, vendor drawings, DFM approval
Phase 2 — Procurement	Long-lead items: exchanger coils, glycol pumps, scanner system, control panel	6-8 Weeks	Material test certificates, QC inspection reports, FAT invitation
Phase 3 — Fabrication	Exchanger skid fabrication, ductwork sections, control panel assembly	6-8 Weeks	Factory Acceptance Test (FAT) at KERONE Ambarnath; client witness invited
Phase 4 — Installation	Equipment erection during scheduled mill shutdown; ducting, electrical, instrument hook-up	2-3 Weeks	KERONE site supervision; civil and electrical by client as per KERONE drawings
Phase 5 — Commissioning	Cold trials, hot trials on running PM-1, performance guarantee test, operator training	1-2 Weeks	Commissioning report, performance test certificate, O&M manual, training records
TOTAL PROJECT TIMELINE	Order to commercial operation	~23-31 Weeks	From purchase order to first verified performance test

KERONE Scope of Supply & Services

Category	KERONE Scope (INCLUDED)	Client Scope (EXCLUDED from KERONE supply)
Process Design	Process design basis, mass & energy balance, P&ID	Feedstock (paper furnish) quality guarantee; mill operating schedule
Primary Equipment	Heat recovery exchanger, hood modification, flash vessel, scanner system	Existing dryer cylinders, press section, reel (unmodified)
Controls	PLC/SCADA integration, all new instruments and field wiring	Existing DCS licensing, main power supply connection, transformer
Civil & Structural	Foundation load drawings, GA layout, anchor bolt drawings	All civil work, ductwork supports, scaffolding, platforms
Commissioning	FAT, site commissioning, performance test, operator training (10 days)	Consumables (steam, glycol top-up) for commissioning; paper stock for trials
Documentation	P&ID, GA drawings, O&M manual, spares list, test certificates	Client-side approvals, regulatory consents, insurance

Conclusions & Why KERONE

The KERONE-designed dryer section retrofit for Shree Ganesh Paper & Boards Ltd. represents a proven, commercially validated solution to one of the most significant energy-cost reduction opportunities available on an existing paper machine. The design is built on rigorous KRDC on-site trial data — not theoretical projections — and the industrial design directly replicates the exact process conditions that produced measurable, certified results on the client's actual production dryer section.

- **Proven Technology** — Every process parameter in the retrofit design — 4-zone graduated steam pressure profile, 65% hood heat recovery — is directly derived from KRDC on-site trial 52/KRDC/LAB/22 on the client's actual PM-1. No extrapolation; no assumptions.
- **Quantified Outcome** — Specific steam consumption reduction from 1.92 to 1.45 kg/kg, and exit moisture uniformity improvement from $\pm 1.2\%$ to $\pm 0.3\%$, are measurable, instrumented results — not marketing claims.
- **Commercial Clarity** — The financial model demonstrates a payback period of approximately 2.3 years at the client's current fuel cost basis, converting an existing energy liability into a INR ~2.6 Cr/year net benefit line.
- **Full Ownership** — KERONE designs, manufactures, supplies, installs, and commissions the complete retrofit from a single point of accountability — eliminating multi-vendor coordination risk during a live mill shutdown.
- **Scalable Platform** — The heat-recovery and pressure-profiling methodology validated at Shree Ganesh Paper & Boards creates the reference installation for retrofits on other paper machines of 100-500 TPD capacity across India and internationally.
- **Compliance-Ready** — The design reduces specific CO₂ emissions per tonne of paper by ~24%, directly supporting the client's ESG reporting to FMCG brand-owner customers.

ENQUIRE ABOUT YOUR PAPER MACHINE DRYER SECTION UPGRADE

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To initiate a project discussion, please share: dryer section drawings + steam & fuel cost data + machine speed/grade profile + site location

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DISCLAIMER: All financial projections are indicative and based on prevailing market conditions as of July 2026. Process performance figures are derived from KRDC on-site trial data (Report 52/KRDC/LAB/22) conducted on Shree Ganesh Paper & Boards Ltd. feedstock and operating conditions. Actual industrial performance may vary. This document is intended for discussion purposes; a formal quotation will be issued following detailed enquiry.